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Cyclic Carbonates from Carbon Dioxide and Oxiranes

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The synthesis of cyclic carbonates 2 by reaction of carbon dioxide with oxiranes 1 in the presence of alkali metal salt-phase-transfer agent catalysts is reported. A reaction mechanism is proposed.

(Keywords: Crown ether; Phasetransfer catalyst)

Synthesen cyclischer Carbonate aus $CO₂$ *und Oxiranen*

Synthesen cyclischer Carbonate 2 durch Umsetzung von CO₂ mit Oxiranen 1 in Gegenwart yon Alkalimetall-Phasentransfer:Katalysatoren werden beschrieben. Ein möglicher Reaktionsmechanismus wird vorgeschlagen.

Introduction

The chemistry of carbon dioxide has received much attention in recent years. It has been considered as a monomer in polymerization and polycondensation reactions, which have been reviewed elsewhere¹. Attention has also been paid to its reaction with epoxides leading to cyclic alkylene carbonates. From these carbonates polymeres having ester² as well as carbonate and ether³ linkages were synthesized.

The literature reports^{$4,5$} on the synthesis of alkylene carbonates by the $CO₂$ reactions with oxiranes in the presence of various catalysts, such as quaternary ammonium and alkali metal salts or some other metal derivatives. These reactions, however, do not proceed under mild conditions in high yields and, when catalyzed by transition metal complexes, they were accompanied in some cases by oxirane homopolymerization⁶. However, in the case of the nickel (0) phosphine complexes they produced cyclic carbonates in rather high yields⁵.

Although alkali metal salts appeared to be rather poorly active

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catalysts for the CO_2 -expoxide reaction, the introduction of a crown ether or another phase-transfer agent to the system could be expected to enhance their catalytic activity. This could cause the activation of the respective anion to such an extent that the cyclic alkylene carbonate was produced in a high yield under mild conditions. We sueeeded recently in convenient syntheses of linear carbonate monomers by reactions of CO₂ with alkali metal alkoxide and α,ω -dihalocompounds⁷, as well as alkali metal carbonate with alkyl halides⁸, promoted by anion activating agents. In the present work an attempt has been made to react carbon dioxide under mild conditions with epoxide compounds in the presence of catalytic systems composed of the alkali metal salt and the anion activating agent.

Results

By selecting the conditions and catalysts, the $CO₂$ reaction with epoxides 1 (Tables 1-5) proceeds according to Eq. (1). The structures of the products (a cyclic carbonate 2) was confirmed by elemental analysis as well as by IR and 1H-NMR spectroscopy.

The effect of the catalyst on the yield of 4-chloromethyldioxolone-2 (2e) formed from the reaction of $CO₂$ with epichlorohydrin (1e) was investigated.

Table 1 shows that the above reaction proceeds in the presence of alkali metal halides and carbonates with relatively low yields (up to ca. 30%). The use of a crown ether for the alkali metal causes a remarkable

Catalyst system	Yield of 2e ^b ℅		
$\rm Na_{2}CO_{3}$ -15-crown-5	95		
K_2CO_3	7		
$K_{2}CO_{3}$ -18-crown-6	98		
LiCl	24		
NaCl	26		
KСl	32		
$LiCl$ — 15 -crown- 5	36		
$NaCl—15-crown-5$	89		
KCl--18-crown-6	93		
КT	29		
$KI-18$ -crown-6	97		
$CH3COOK-18-cor$	83		
$L-(+)$ -KOOC[CH(OH)] ₂ COOK-18-crown-6	84		
C_eH_eOK-18 -crown-6	82		

Table 1. *Yield of 4-chloromethyldioxolone-2* 2e in the reaction of $CO₂$ with epichlorohydrin I e in the presence of alkali metal salt-crown ether catalytic *systems ~*

^a Reaction conditions: **l** e, 0.18 mol, CO_{2} initial pressure 40 atm; alkali metal salt, 1.2 mmol, crown ether, 0.38 mmol; temp. 120 °C, time 24 h.

^b Calculations based on **I** e.

increase in the yield of 2 e, which in some cases, e.g. in the presence of potassium carbonate or iodide and 18-crown-6 ether reaches almost 100%. The reaction of $CO₂$ with 1e proceeds also with high yield in systems containing crown ether and other alkali metal salts as catalysts such as potassium carboxylates and phenolates.

The reactions of $CO₂$ with oxiranes without halomethyl substituents at the ring in the presence of the alkali metal carbonate--crown ether catalyst proceeds with very low yields of $2(1-2%)$. Also in the presence of alkali metal carboxylates activated by a crown ether these reactions did not proceed. On the other hand, when alkali metal bicarbonate or phenolates with a crown ether as catalyst were applied, the reaction of CO₂ with an oxirane without a halomethyl substituent at the ring gave 2. However, the yield of 2 in these reactions was much lower than in the analogous reaction of $CO₂$ with epihalohydrin. These results are illustrated by the reaction of several oxiranes I b, d, k, given in Table 2. Taking into account the higher activity of the potassium carbonate-crown ether catalyst in the reaction of $CO₂$ with epihalohydrin than with the other epoxy compounds studied, an analysis of the catalyst remaining in the mixture was carried out:

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Epoxide compound 1	Potassium salt	Reaction temp. °C	Yield of 2^b $\%$		
1 b	$K_{\rm s}CO_{\rm s}$	120	2		
	$\mathbf{KOOC}(\mathbf{CH_2})_8\overset{\circ}{\mathbf{COOK}}^\mathrm{c}$	120	7		
		80	traces		
	C_6H_5OK	120	12		
	$2{,}4{\cdot}(\tilde{\hbox{NO}}_2)^2_2\tilde{\hbox{C}}_6\hbox{H}_3\hbox{OK} \ \hbox{K}_2\tilde{\hbox{CO}}_3^3 \ \hbox{K}_2\tilde{\hbox{CO}}_3^3$	120	5		
1 d		120			
1e		70	32		
		80	68 ^d		
		100	91 ^d		
		120	98		
		130	92		
1g		80	96		
1 k	$\frac{\textrm{K}_2\textrm{CO}_3}{\textrm{K}_2\textrm{CO}_3}$	120	ı		

Table 2. *Yield of cyclic carbonate* 2 *in the reaction of* CO _{*a} with the epoxide* 1 *in the*</sub> presence of the potassium salt-18-crown-6 ether catalytic systems^a

Reaction conditions: 1, 0.18 mol, $CO₂$ initial pressure 40 atm, potassium salt, 1.4 mmol, 18-crown-6, 0.38 mmol, time 24 h.

b Calculations based on 1.

 $\frac{\rm c}{\rm c}$ 1 b, 0.25 mol, potassium salt, 0.8 mmol, 18-crown-6, 0.19 mmol.

 u Alkali metal salt, 1.2 mmol.

Table 3. *Effect of the structure of epoxide 1 on the yield of the cyclic carbonate 2 in the reaction of* CO_2 *with* 1 in the presence of the KI-18-crown-6 ether catalytic system^a

Epoxide compound 1					a b b^c c d e f^d g h i j	
Yield of 2^b %					91 90 95 25 68 97 92 96 73 90 90	- 75

^a Reaction conditions: 1, 0.18 mol, CO₂ initial pressure 40 atm, KI, 1.2 mmol, 18-crown-6, 0.38 mmol, temp. 120° C, time $4 h$.

b Calculations based on 1.

 $^{\circ}$ Temp. 100 $^{\circ}$ C, time 24 h.

 μ 1, 0.1 mol, temp. 90 °C, time 24 h.

In the reaction with epihalohydrin 1 e a large amount of KC1 (with respect to K_2CO_2) was found. It follows that K_2CO_2 activated by the crown ether reacts with I e giving KC1, which in a finely dispersed state with the crown ether is a very active catalyst for the reaction of CO₂ with 1 e. The reaction of CO₂ with 1 e in the presence of $L(+)$ tartaric acid and crown ether as catalyst yields optically inactive 2 e. This confirms the mechanism, in which the reaction is catalyzed by the *in situ* formed KCl being of course optically inactive.

Phase-transfer agent	2e				
	Amount		Amount	${\rm Yield}^{\rm b}$	
	g	mmol	g	$\frac{9}{6}$	
18 -crown-6	0.1	0.38	24.2	97	
$DB-18$ -crown-6	0.1	0.27	23.2	93	
15 -crown-5	0.1	0.45	24.2	97	
DABCO	0.1	0.9	23.7	95	
TMEDA	0.2	1.7	23.0	92	
Polyglyme 300	0.75	2.5	8.3	33	
Polyglyme 600	0.75	1.24	15.5	62	
Poly(ethylene glycol) 1500	1.0	0.67	11.2	45	
TERA	0.2	0.88	22.7	91	

Table 4. *Relationship between the kind of the phase-transfer agent and the yield of 4chloromethyldioxolone-2* 2 e in the reaction of CO , with epichlorohydrin 1 e in the presence of KI-phase-transfer agent catalytic systems^a

^a Reaction conditions: 1e, 16.6g, 0.18 mmol, $CO₂$ initial pressure 40 atm, KI, 0.2g, 1.2mmol, temp. 120°C, time 24h.

b Calculations based on 1e.

Table 3 presents the yields of cyclic carbonates $2a-k$ in the reactions of $CO₂$ with epoxy compounds in the presence of the catalytic system KI--18-crown-6 at 120 °C within 4h. The highest yields of 2 were obtained in the reaction with $1 e^{-g}$. High yields of 2 (ca. 90%) were also obtained in the reaction of CO₂ with n-butyl- and allylglycide ethers (1i, j) as well as with ethylene and propylene oxides $(1a, b)$. Phenyl derivatives, e.g. styrene oxide $(1 d)$ and phenylglycide ether $(1 k)$ gave 2 in ca. 70% yield, but the 2,3-disubstituted cyclohexene oxide 1 c gave the cyclic carbonate in low yields (of only 25%).

From these studies (Table 2) it appears that the reaction of $CO₂$ with the epoxy compound proceeds with the highest yields of 2 at 120 °C. A decrease of the reaction temperature causes a considerable decrease in the yields of the cyclic carbonate. Above 120 °C, however, the yield of 2 decreases somewhat resulting from side reactions (opening of the dioxolon ring in 2 by the catalyst⁹). In the reactions both of epihalohydrins as well as of other epoxides at various temperatures no oxirane homopolymers or $CO₂$ -oxirane copolymers were found. Due to the lack of side products in the reactions of $CO₂$ with epoxides, the catalyst recovered by distilling 2 from the reaction mixture could be reused.

The yield of 2 depended to a great extent on the agent activating the catalyst. Instead of the crown ether, also other phase-transfer agents, such as 1,4-diazabieyclo-[2,2,2J-octane *(DABCO), N,N,N,N-tetra*methylethylenediamine *(TMEDA)* and also triethylbenzylammonium chloride *(TEBA)* could be used for the CO_s/e poxide reaction and give rise to a high conversion of $CO₂$ and the oxirane to the cyclic carbonate.

 $Table 5.~\,Relationship~\, between~\,the~\,CO_2~\,pressure~\,and~\,yield~\,of~\,4$ *chloromethyldioxolone-2* 2 e in the reaction of $CO₂$ with epichlorohydrin 1 e in the presence of the KI--18-crown-6 ether catalytic system[®]

$CO2$ initial pressure atm	1 _{b,c}	6°		16	30	40
Yield of $2e^d$ %		76	54	85	91.5	97

^a Reaction conditions: 1 e, 0.18 mol, mole ratio CO₂/1 e = 1.5, KI, 1.2 mmol, 18-crown-6, 0.38 mmol, temp. 120° C, time 24 h.

^b Constant pressure during the reaction.

 $\frac{\text{e}}{\text{}}$ Temp. 116 °C.

^d Calculations based on **1e**.

For example, in the case of 2e the conversion was higher than 90% (Table 4). Polyglymes and poly(ethylene glycol) were also found to play the role of a phase-transfer agent. However, the yield of 2e are much lower (ca. $30-60\%$) (Table 4).

The yield of the cyclic carbonate 2 depends also on the $CO₂$ pressure in the reaction system. The yield is near to the theoretical at an initial pressure of 40 bar. However, when a comparatively low but constant $CO₂$ pressure during the reaction (of ca. 6 bar in the case of 1e) is maintained, the yield of 2 is relatively high (Table 5).

Discussion

As appears from the results presented, the catalytic activity of alkali metal salts in the reaction expressed by Eq. (1) increases with an increase in the anion nucleophilicity and cation diameter. Complexation of the cation by a crown ether, *DABCO, TMEDA* or another phase-transfer agent, such as *TEBA,* facilitates the nucleophilic attack of the anion on the oxirane ring. In this work no simple correlation was found between the reactivity of oxiranes in the reaction (1) and their tendency to form hydrogen bonds¹⁰. However, it seems that such an attack of the anion toward the oxirane ring could be facilitated due to donor--acceptor interactions between the oxirane ring oxygen atom and the cation. Due to a considerable excess of the oxirane with respect to the crown ether in the systems studied, an oxirane interaction with the cation is possible, despite the stronger bonding of the cation by the ether. Such an interaction causing a decrease in electron density in the oxirane ring is more probable, since the reactions are carried out without a solvent which could compete with oxirane in the cation solvation. The oxirane ring opening due to the attack of the $X^$ anion can take place by the cleavage of the CH₂—O or CH—O bonds, depending on the kind of substituent R at that ring¹¹. After opening of the oxirane ring and formation of a new alcoholate anion, according to Eq. $(2a, b)$ the CO₂ addition to that anion with the formation of a carbonate anion according to Eq. $(3 a, b)$ takes place. This is followed by subsequent dioxolone ring formation (Eq. 4 a, b). The above reactions reflecting the proposed mechanism of formation of cyclic carbonate 2 from $CO₂$ and oxirane 1 are illustrated in the following scheme:

 K^+ = crown-ether complex.

In the systems studied the intermediate product of reaction $(2a, b)$ (alcoholate-anion) does not undergo further reaction with the oxirane where poly- (alkylene oxide) could be formed. This results from the greater stability of the alkyl carbonate anion formed in the reaction (3 a, b) than that of the initial alcoholate anion; thus this latter anion reacts easier with $CO₂$ (3 a, b) than with the oxirane. However, the oxirane polymerization products are formed in systems not containing $CO₂$ and when alkali metal salts giving not very strong nueleophiles (such as potassium carbonate, potassium monoalkyl carbonate, potassium carboxylate) activated with a crown ether are used l^2 . In the systems studied also no poly(alkytene carbonate) is formed from the intermediate alkyl carbonate anion obtained in the reaction (3 a, b). This probably results from the anchimerie assistance taking place, and also due to the greater thermodynamic stability of the five-membered dioxolone ring formed from the cyclization of that anion (Eq. 4a, b) with respect to the linear polycarbonate. Poly(alkylene carbonate)s can be obtained in the alternating copolymerization of $CO₂$ with oxiranes in the presence of coordination catalysts, the mechanism of which has been described elsewhere 13 .

Experimental Part

The epoxides $1 a, b, d-f$, i-k were of commercial grade, $1 c$ was obtained from the reaction of cyclohexene brom0hydrin with a water solution of sodium hydroxide, \lg from that of 1,3-dibromopropanol-2 with calcium hydroxide¹⁴ and 1 h from that of 3-chloropropandiol-l,2 with phenylglycidyl ether in the presence of *TEBA* 15. The epoxides 1 were dried prior to use by known methods. The alkali metal halides and carbonates were used after powdering and drying at 120 °C *in vacuo.* Potassium phenolates and carboxylates were obtained in known reactions with potassium hydroxide, applying azeotropic distillation to remove water from the reaction medium, and then dried at 130°C *in vacuo.* Crown ethers: 18-crown-6 (1,4,7,10,13,16-hexaoxacyclooctadecane) and 15-crown-5 (1,4,7,10,13-pentaoxacyclopentadecane) were obtained as described in the literature 16. Polyglymes were obtained from the reaction of the sodium salt of the respective poly(ethylene glycol) (commercial grade) with ethyl bromide. *TEBA,* commercial grade, *DABCO* and *TMEDA,* Fluka AG, were used without further purification.

General Procedure

To a 60 ml stainless steel pressure cylinder 1 and a respective amount of the catalyst were introduced, and then CO_2 from a gas cylinder was added at a ca. 1.5-fold greater amount by mole than 1. The pressure cylinder was then closed and placed in a thermostated oil bath. In some cases $CO₂$ was introduced to the reactor under constant pressure during the reaction from a 401 cylinder of a given CO₂ pressure. After completion of the reaction the pressure cylinder was cooled to room pressure, the excess of $CO₂$ was liberated and the product formed was washed to remove the catalyst with 10 ml of water (with the exception of 2a) and then distilled under reduced pressure. The yield of 2 was determined gravimetrically. The cyclic carbonates 2 obtained were characterized by means of elemental analysis (Perkin-Elmer model 240 microanalyser), ¹H-NMR spectroscopy (JEOL-C 100 H spectrometer, *TMS* being used as internal standard) and IR spectroscopy (film, Specord 71 IR-GDR). Boling or melting points (uncorrected), density and refractive index were also determined for those carbonates 2 (Table 6).

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